



**Shell Global Solutions**

# Use of Predictive Models in Vapor Intrusion Investigations

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*Vapor Intrusion - The Next Great Environmental Challenge*

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M. A. Lahvis, Shell Global Solutions (US), Inc., 13, September, 2006

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# Overview

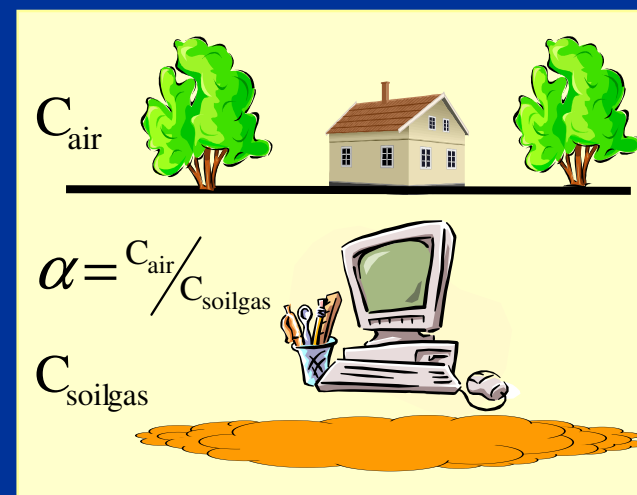
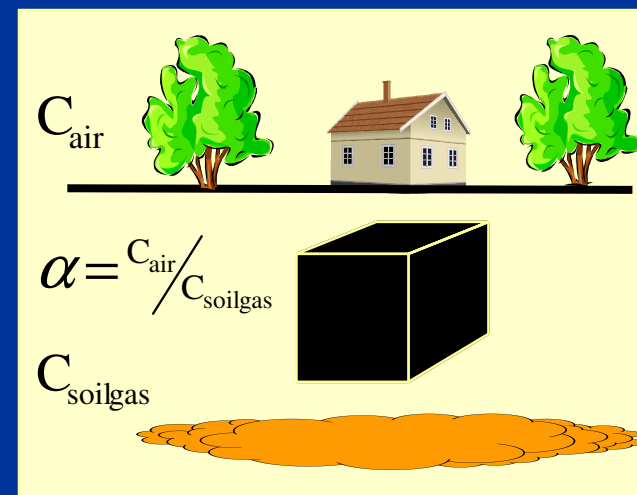
## ■ PART I

Issues with the Use of Predictive Models

## ■ PART II

Predictive Model for Screening Dissolved-Phase Petroleum Hydrocarbon Sites

## ■ Summary



# Issues

## POSITIVES

- models if used properly, can help:
  - guide SIs (identify sensitive parameters), avoid unnecessary sampling
  - identify relevant transport processes
  - quantify unknowns
  - predict uncertainties



# Issues (Cont'd.)

## NEGATIVES

- processes governing VI can be highly variable and are not easily quantified
  - nobody expects models to predict the future exactly
    - o what degree of confidence is acceptable? (stakeholder implications)
    - o prediction is only as good as the calibration/validation
- general unfamiliarity with more sophisticated models
- most widely accepted VI models are either too conservative or too simple (i.e., do not account for relevant processes, such as biodegradation)

OK - do we really want to do this?



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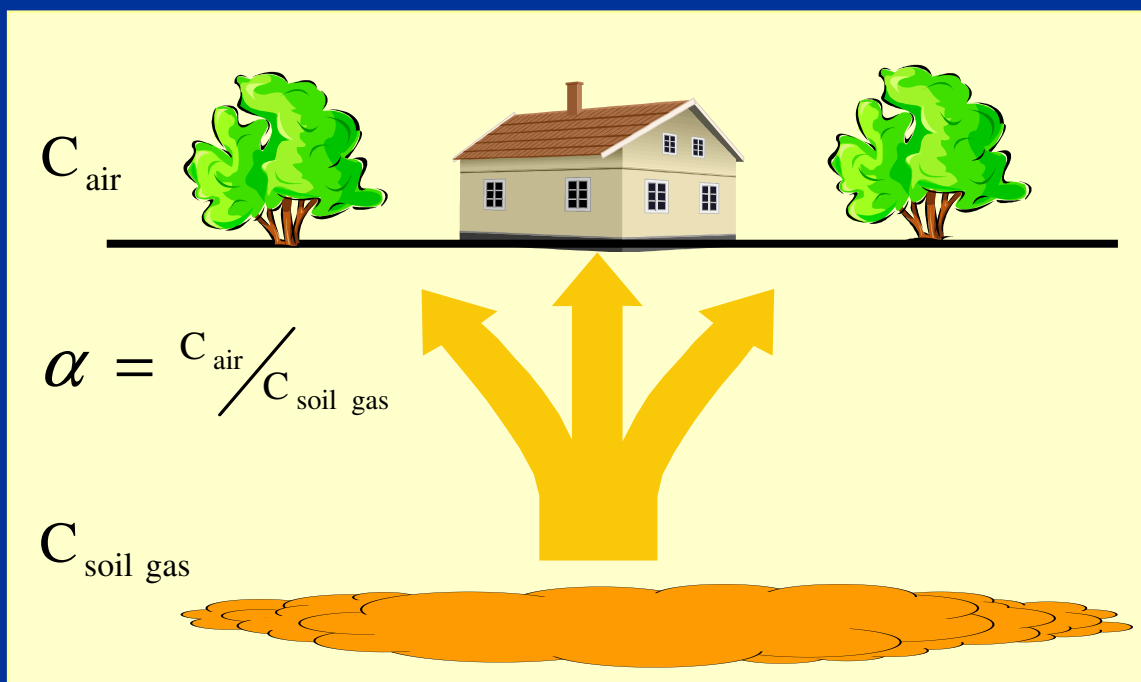
# Issues (Cont'd.)

## MAJOR CONCERNS

- there is a tendency for misuse and abuse of models
- applications beyond simple spreadsheets not generally performed and acceptance generally limited
  - restricted use for site-specific applications



# General Conceptual Site Model (CSM)



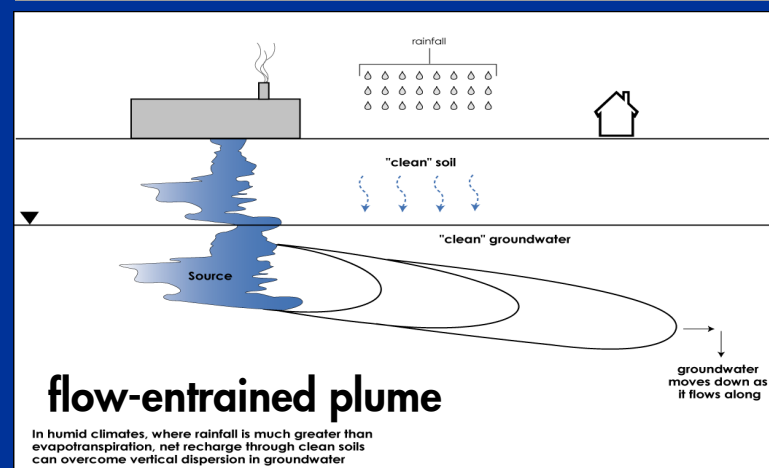
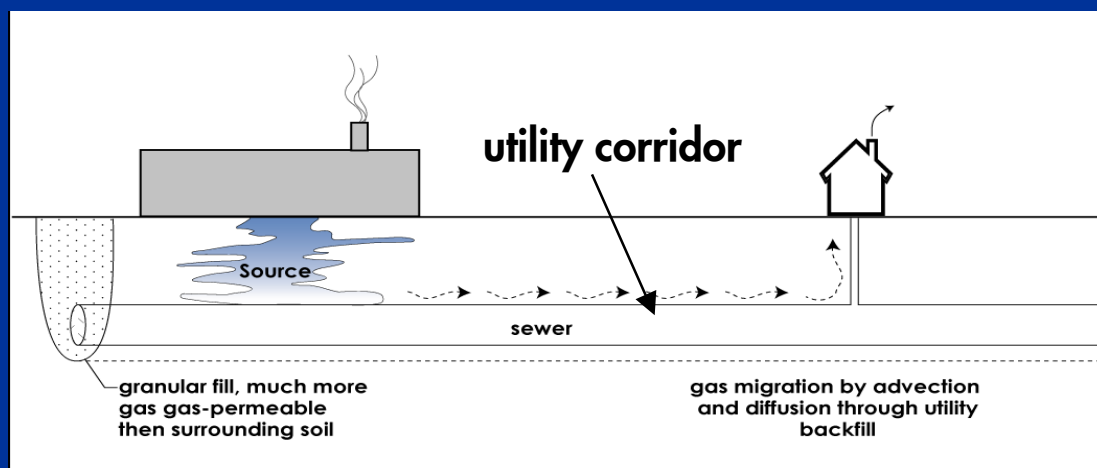
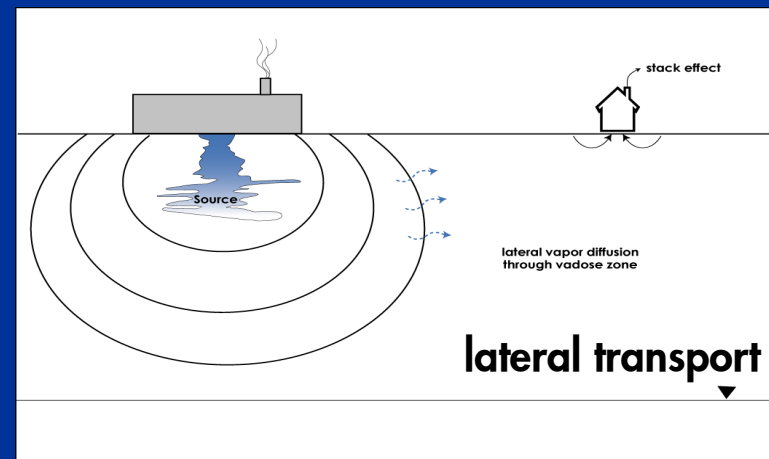
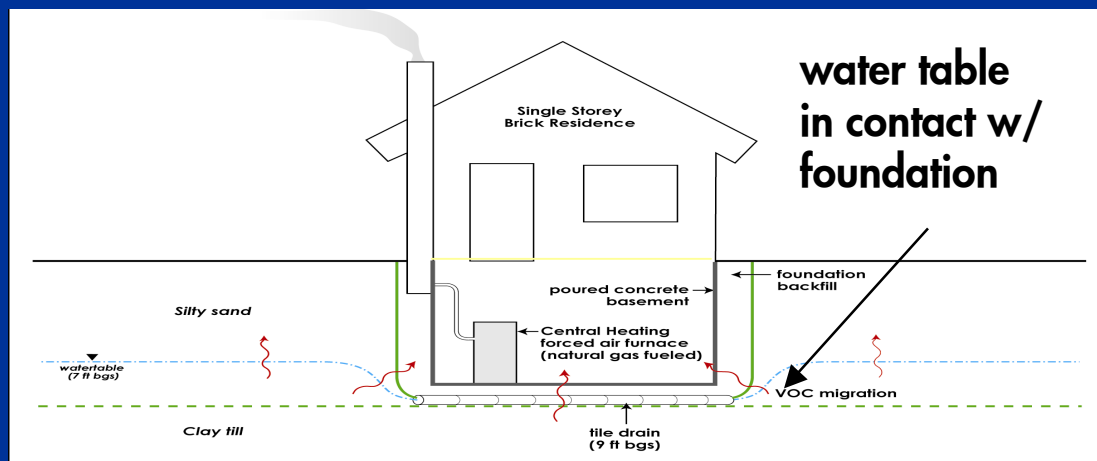
- Mixing in Breathing Zone
- Convective Transport into Bldg
- Diffusive Transport to Breathing Zone
- Impacted Soil and/or Groundwater in Equilibrium with Soil Gas

## KEY POINTS:

- CSM is specific to certain models (e.g., 1-D)
- Important to collect necessary data to determine if model is applicable to CSM

# Factors to Consider in CSM

*Figures courtesy of T. McAlary*



- CSM must be valid for model application
- the predictive calculation is only as good as the investigative process itself

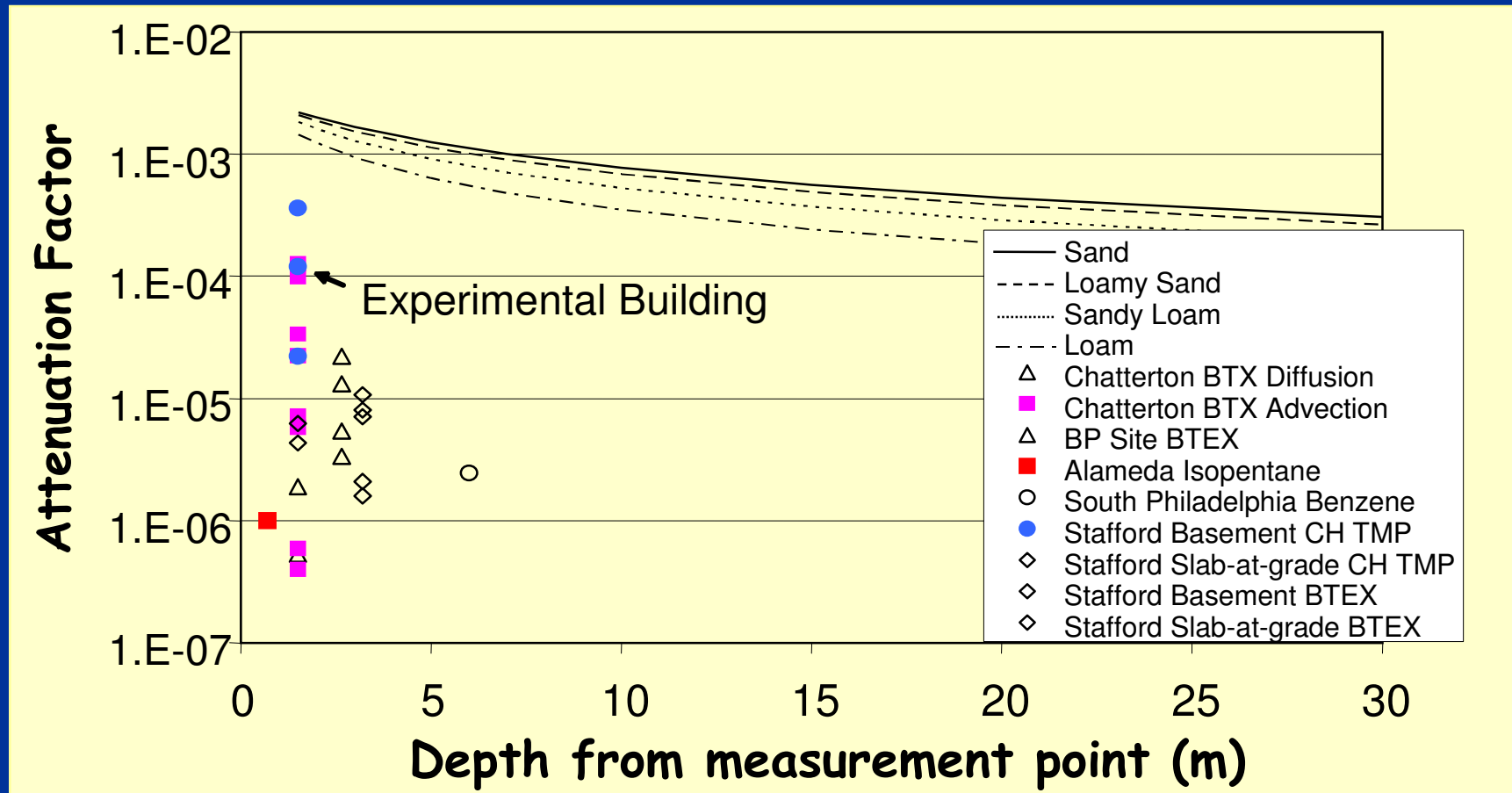
# Model Selection

## Model

Model	Published	1-D Vertical	Multi-Dimensional	Diffusion	Gaseous-Phase Advection	Slab Resistance	Infiltration	Biodegradation	Analytical	Numerical	Transient
Jury et al.	1983/1990	X		X			X	X	X		X
Johnson and Ettinger (1991)	1991	X		X	X	X			X		
Orange County Health Care Agency	1991	X		X		X			X		
Little et al.	1992	X		X	X				X		X
Sanders and Stern	1994	X		X	X			X	X		X
Ferguson et al.	1995	X		X	X	X		X	X		X
Jeng et al.	1996	X		X				X	X		X
R-UNSAT (Lahvis and Baehr)	1997	X	X	X			X	X	X	X	X
Krylov and Ferguson	1998		X	X	X			X	X	X	
Dominant Layer Model (Johnson et al.)	1998/1999	X		X	X	X		X	X		
Oxygen Limited Model (Johnson et al.)	2000	X		X	X	X		X	X		
Parker	2003	X	X					X			
Abreu and Johnson	2005		X	X	X	X		X		X	X



# Measured vs. Conservative Model -- Hydrocarbons



- measured AFs for petroleum hydrocarbons can be orders of magnitude less than semi-site specific screening levels

# Screening Model for Dissolved-Phase Petroleum-Hydrocarbon Sites

## Governing Transport Equation 1-D Vertical (steady-state)

$$D \frac{\partial^2 G}{\partial z^2} - \lambda C = 0$$

diffusion      biodegradation

$D$  = effective diffusion coefficient  
 $\lambda$  = first-order rate constant  
 $C$  = aqueous-phase concentration  
 $G$  = gaseous-phase concentration  
 $z$  = distance

## Transformed Equation (dimensionless analysis)

$$\frac{\partial^2 C}{\partial x^2} - D_m C = 0$$

where,

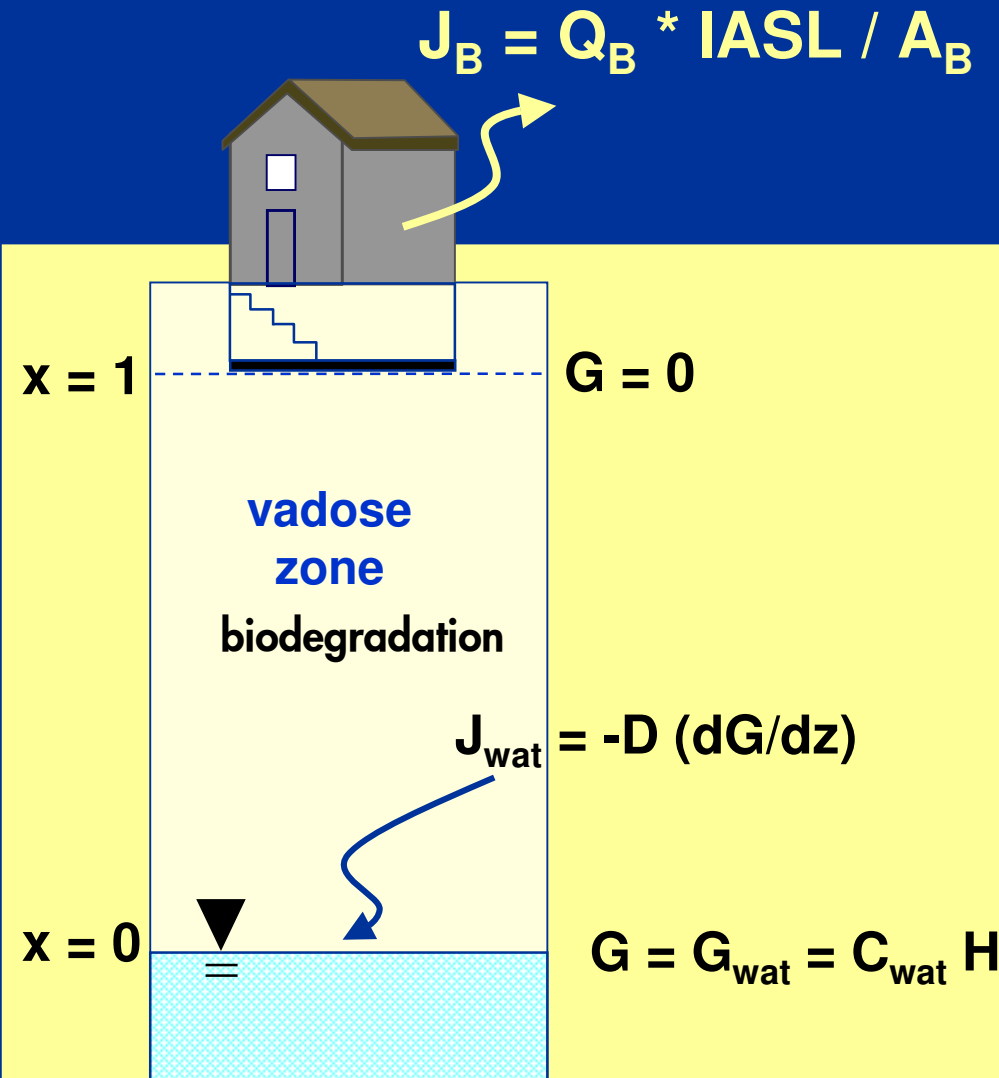
$$D_m = \frac{\lambda L^2}{D H}, \quad x = \frac{z}{L}$$

$D_m$  = scales biodegradation and diffusion

$H$  = Henry's Law constant

$L$  = distance

# Boundary Conditions and Model Assumptions



- 1-D, uncoupled transport (conservation of mass)
- conservative with respect to diffusive transport
  - at  $x = 1, G = 0$
- first-order kinetics
- uniform soil properties - weighted avg. diffusion coeff.
- equilibrium partitioning
- may not be appropriate for all applications (advection  $\gg$  diffusion)

# General Site-Specific Application: Predict Risk-Based Screening Level (RBSL)

- a) calculate mass flux to indoor air ( $J_B$ ):  $J_B = Q_B * IASL / A_B$
- b) calculate  $D_m$ : typical knowns - depth to groundwater ( $L$ );  
soil type ( $D$ ), Henry's Law ( $H$ );  
typical unknown - biodegradation rate ( $\lambda$ )

## Default Values

$D(\text{benzene}) = 0.12 \text{ m}^2/\text{d}$  (sand, EPA spreadsheet) (Default)

For unsaturated soils and BTEX concentrations in pore water  $< 0.2 \text{ mg/L}$ , kinetics first order apply:

$\lambda$  (avg.) =  $5.8 \text{ d}^{-1}$

$\lambda$  (lower 95%) =  $0.5 \text{ d}^{-1}$

$\lambda$  (default) =  $0.25 \text{ d}^{-1}$

$$D_m = \frac{\lambda L^2}{D H}$$

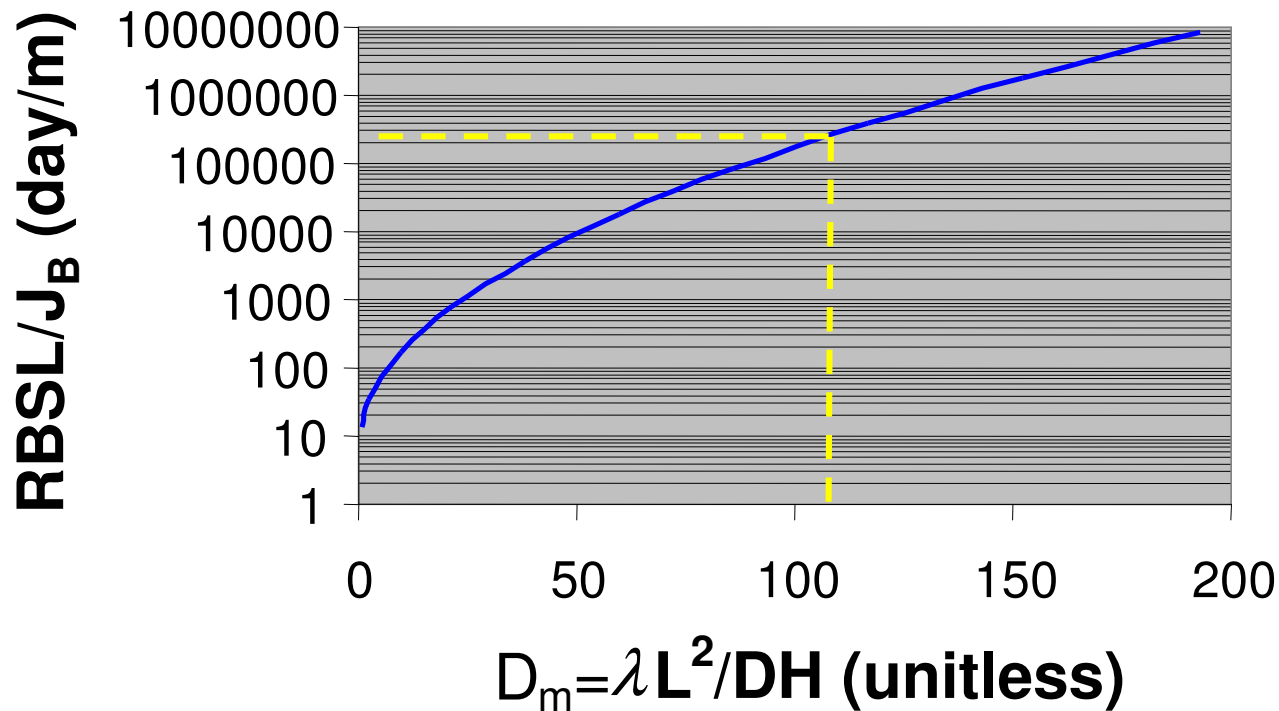
c) apply type curve, determine  $RBSL/J_B$

d) predict RBSL

\* DeVaul et al. (1997)

assumes moisture content = 0.054 (sand, EPA spreadsheet)

# Application Cont'd. (example sand)



- calculate  $J_B$   
( $J_B = Q_B * IASL / A_B$ )

$$Q_B = 2,200 \text{ m}^3/\text{d}$$

$$IASL = 0.23 \text{ } \mu\text{g}/\text{m}^3$$

$$A_B = 100 \text{ m}^2$$

- determine  $D_m$

$$D_m = \left( \frac{\lambda L^2}{DH} \right)$$

$$\lambda = 0.25 \text{ d}^{-1} \text{ (default)}$$

$$L = 3 \text{ m}$$

$$D = 0.12 \text{ m}^2/\text{d}$$

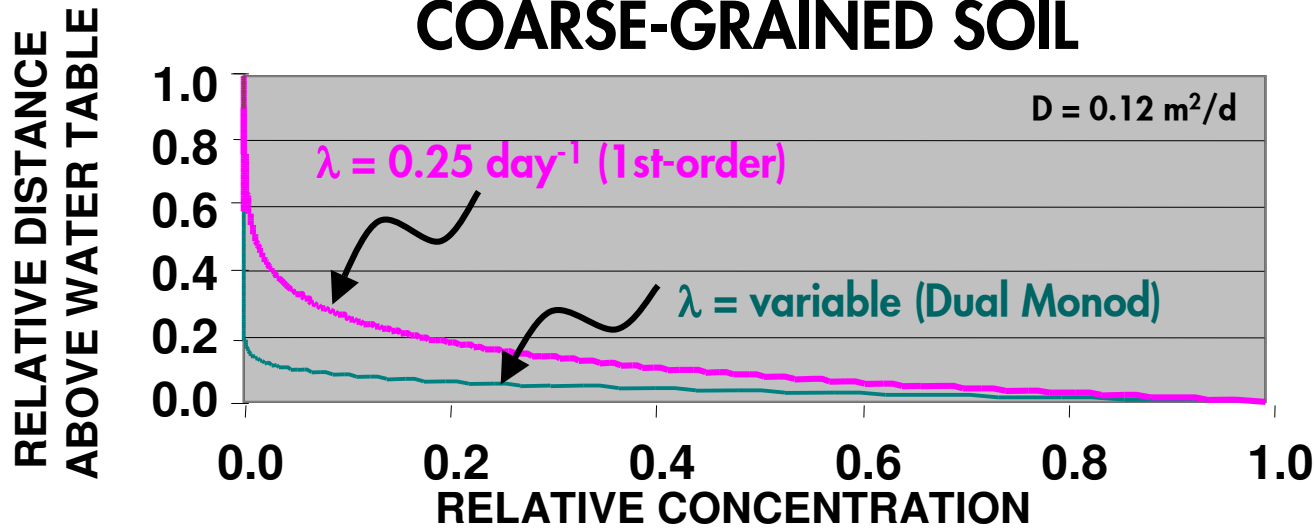
$$H = 0.21 \text{ (benzene)}$$

- determine  $RBSL/J_B$
- calculate  $RBSL$  (ppb)  
( $RBSL = RBSL/J_B * J_B$ )

Biodegradation Rate	<u>0.25 d<sup>-1</sup></u>
$J_B$ (mg/m <sup>2</sup> -d) :	0.005
$D_m$ (unitless) :	110
$RBSL/J_B$ (d/m) :	215,000
$RBSL$ (ug/L) :	1,100

# Validation of 1st-Order Kinetic Model

## COARSE-GRAINED SOIL

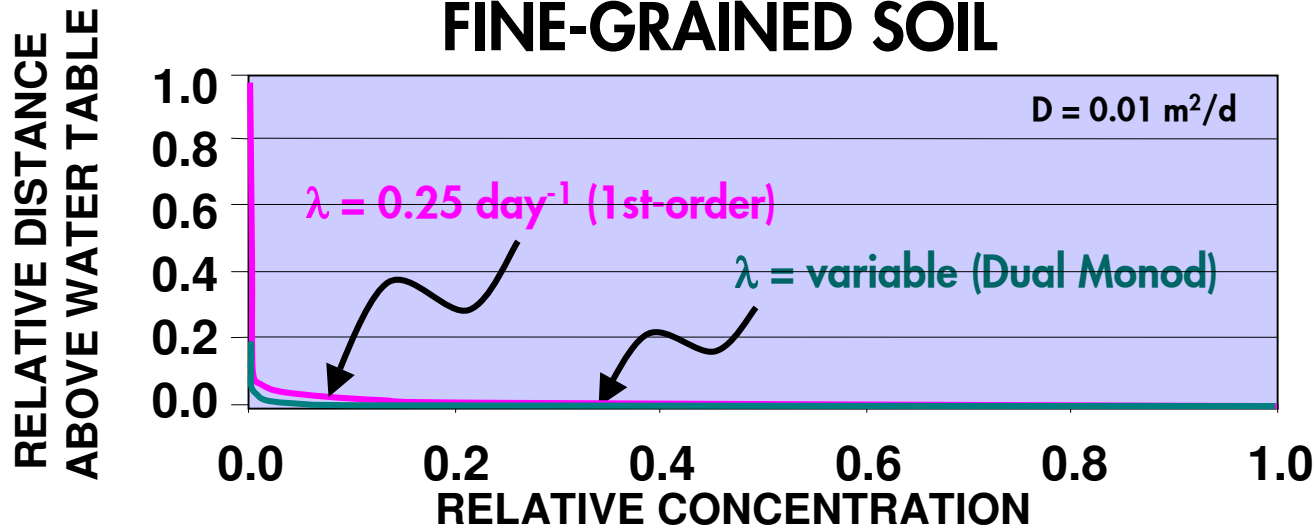


Is 1st-order kinetics assumption ( $\lambda = 0.25 \text{ d}^{-1}$ ) reasonable with respect to potential  $\text{O}_2$  limited biodegradation?

$L = 10 \text{ ft.}$

$C_0 = 1,000 \text{ } \mu\text{g/L}$  benzene

## FINE-GRAINED SOIL



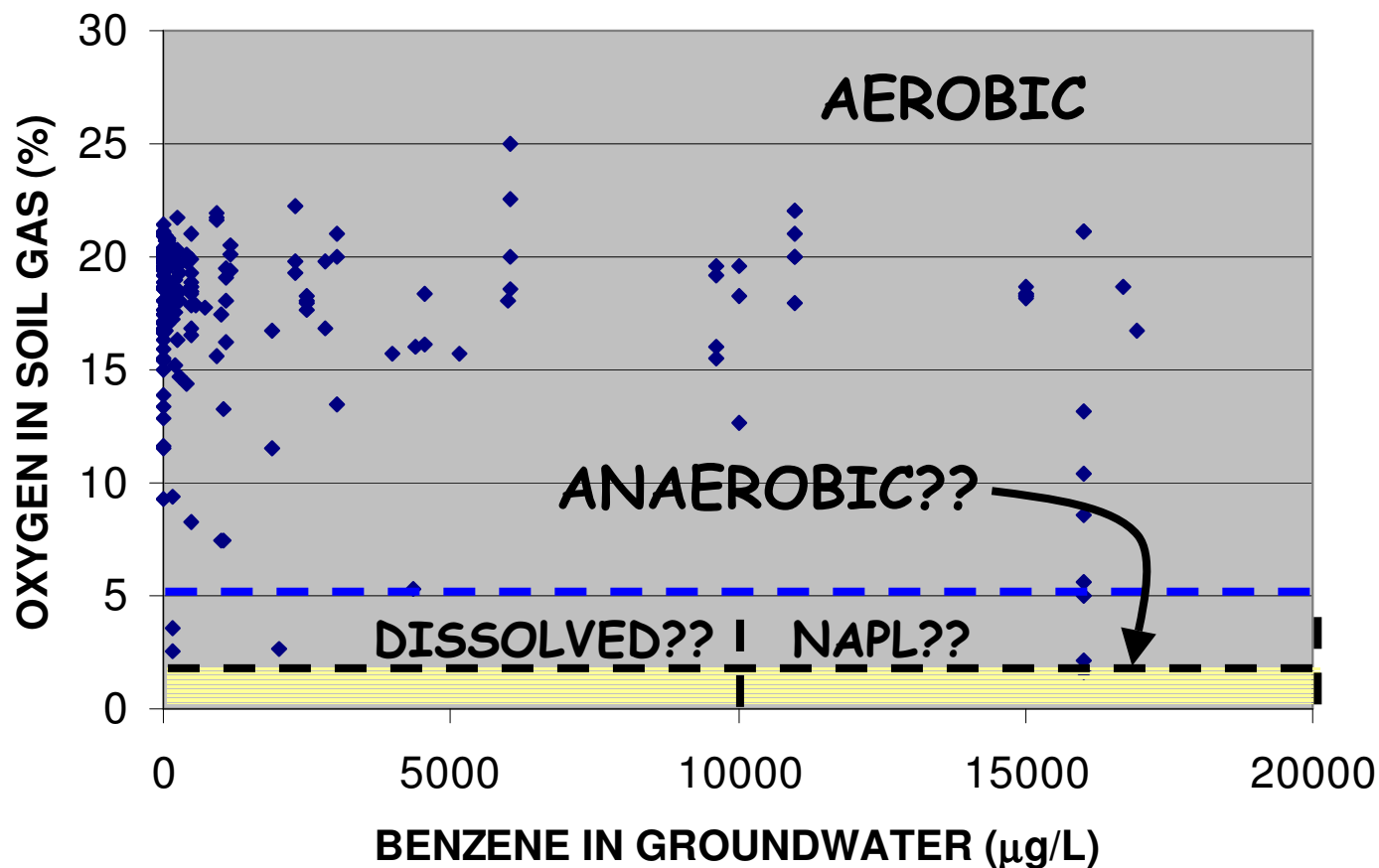
### Dual-Monod Parameters\*

max. rate constant  
=  $0.9 \text{ mg/L-hr}$

half sat. constant  
=  $0.2\text{E-}06 \text{ mg/L}$

*\*from DeVaul et al. (1997)*

# Initial Validation of Biodegradation Parameters

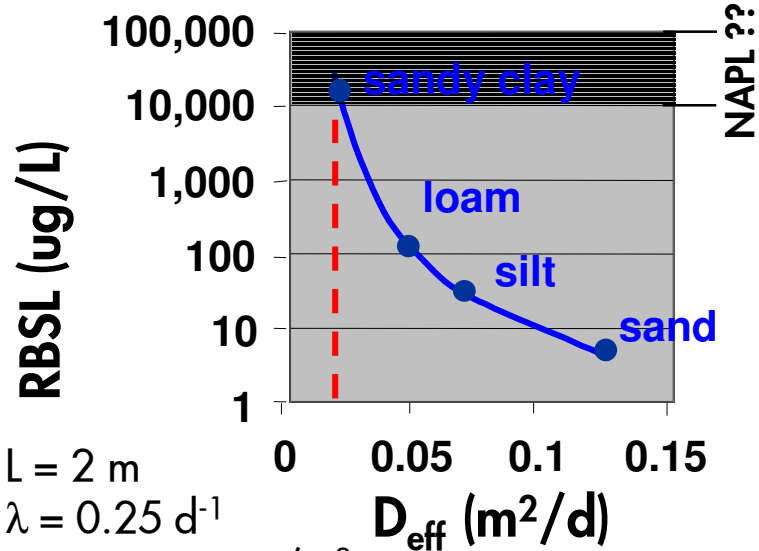


## CO/UT Data Eval.

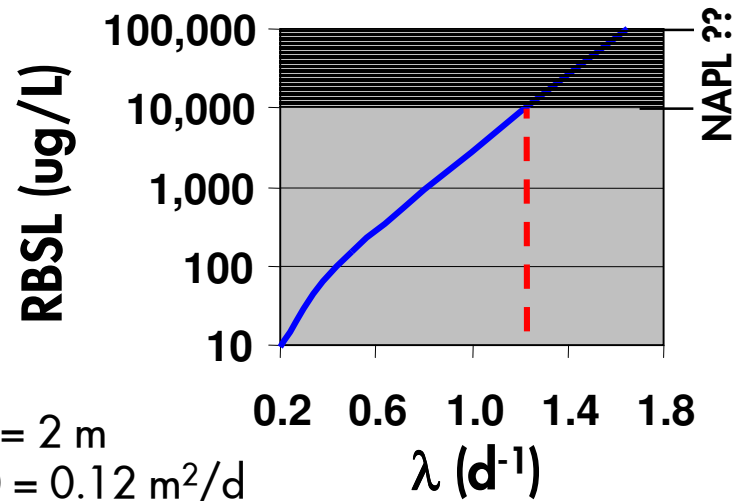
- 5822 soil vapor sampling events, 161 sites
- 696 events ( $O_2/CO_2$  data)
- 447 events w/  
 $O_2 + CO_2 > 18\%$
- 286 events w/  
corresponding GW data
- 3 events (2 wells) w/  
 $2\% < O_2 < 5\%$  (benzene  
 $< 10,000$  ppb)
- 420/447 events w/ BTEX  
concs. in pore water  $< 0.2$  mg/L (not, either  
 $C_{wat}$  benzene  $> 10,000$   
ug/L or UZ source  
implied)

- aerobic conditions are observed in the unsaturated zone for all cases where benzene concentrations in groundwater  $< 10,000$  ppb
- 3 events ( $< 1\%$ ) w/ limited  $O_2$  ( $2\% < O_2 < 5\%$ ) (clay, clayey silt)
- data appear to support 1st-order kinetics at dissolved-phase sites

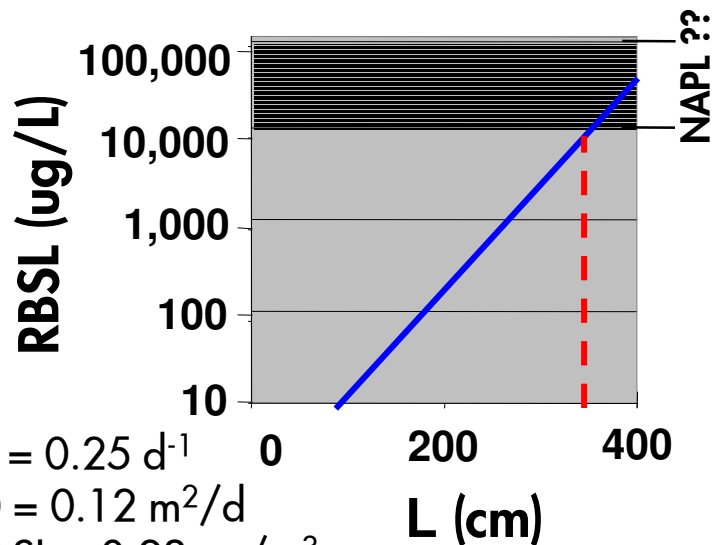
# Parameter Sensitivities



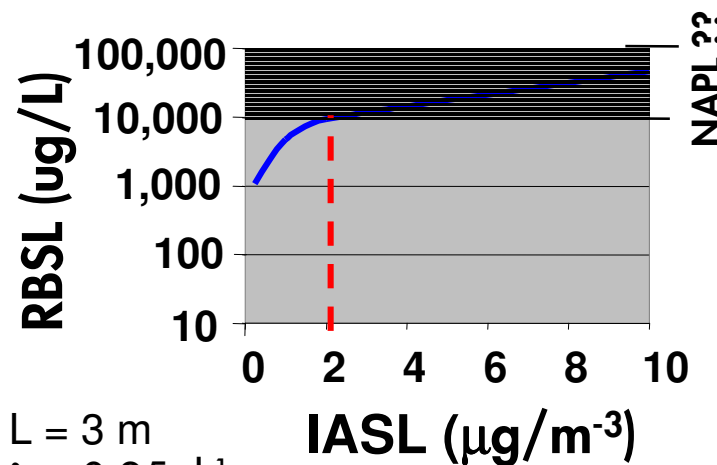
$L = 2$  m  
 $\lambda = 0.25$  d<sup>-1</sup>  
 $IASL = 0.23$  ug/m<sup>3</sup>



$L = 2$  m  
 $D = 0.12$  m<sup>2</sup>/d  
 $IASL = 0.23$  ug/m<sup>3</sup>



$\lambda = 0.25$  d<sup>-1</sup>  
 $D = 0.12$  m<sup>2</sup>/d  
 $IASL = 0.23$  ug/m<sup>3</sup>



$L = 3$  m  
 $\lambda = 0.25$  d<sup>-1</sup>  
 $D = 0.12$  m<sup>2</sup>/d

- sensitivities to  $\lambda$ ,  $L$ , and  $D$  (fine-grained soil) imply AF is highly variable
- consistent with initial database analyses
- exclusion criteria (i.e.,  $L = 3.5$  m) more rational approach than "bioattenuation factor" at dissolved-phase sites



# Summary

- if used appropriately, models can be extremely beneficial in guiding VI investigations (data collection)
- modeling is not appropriate without a basic understanding of the CSM (1-D transport)
- more sophisticated models (as opposed to conservative software) can be extremely helpful in refining predictions and limiting uncertainties, provided:
  - model assumptions and limitations are realized
  - sensitivities are sufficiently characterized
  - adequate field data is available to support application
  - bounds are placed on unknowns with significant variability



# Summary (Cont.'d)

- for petroleum hydrocarbons, meaningful screening levels can only be established by accounting for biodegradation, especially at dissolved-phase only sites
- use of conservative 1st-order rate constant in screening-level model supported by initial evaluation of hydrocarbon database ( $> 2\% \text{ O}_2$  present, BTEX concs.  $< 200 \mu\text{g/L}$ )
- application of screening model indicates current screening levels for benzene are far too conservative for dissolved-phase sites
- analysis indicates exclusion criteria (i.e.,  $L = 3 \text{ m}$ ) is likely better approach than "bioattenuation factor"

